Changes for DDBSP 2015 Update2

Release Date: August 21, 2015

DDBSP 2015 Update2 includes all changes of DDBSP 2015 Update1 (see below).

Flash Point Calculation

New: allow calculation even if heat of combustion is missing

Mixture Prediction / Process Synthesis / Predictive EOS

• Fixed: PSRK/VTPR prediction for private components fails with group assignment error

Mixture Prediction / Process Synthesis / RecPar

- Fixed: Antoine Low / Auto / Best Match do not consider parameter priority
- Fixed: Antoine-Constants defined in Private.pcp are not used in calculations

Mixture Calculation / Process Synthesis / GC2gE

Fixed [NTPRDGPAR] * Regression in version 2015 *: in the parameter selection dialog (load/store) the grid does not autosize
rows

Mixture Prediction

- Fixed * Regression in version 2015 *: last project file for thermo extension v1 is no longer updated
- Fixed [LLE Prediction]: the specified pressure value in transferred to the EOS with factor 1000
- Fixed [USD Thermo Extension]: the calculation fails with "Unknown Error" if there is an uninitialized stream in any (sub)flowsheet

RecPai

• Fixed: the text "Parameters shown in [K]" is wrong

Changes for DDBSP 2015 Update1

Release Date: June 22, 2015

Basic Version

• Fixed [XEditor] * Regression in version 2015 *: the default property/unit for added purities may be wrong

Basic Version / Mixture Prediction

• New: support for Aspen V8.8 added

Mixture Prediction / Process Synthesis

• Fixed * Regression in version 2015 *: the calculation of ternary LLEs with PSRK and VTPR fails

Mixture Prediction / Predictive EOS

• Fixed * Regression in version 2015 *: the text output of EOS alpha function parameters contains max. one value (C1)

Mixture Prediction

- Fixed [LLE Prediction] * Regression in version 2015 *: the text "Lower Limit" appears twice in temperature range area
- Fixed [ELE Prediction] * Regression in version 2015 *: the calculation with LIFAC fails
- Fixed [ESLE Prediction]: the calculation with LIFAC fails
- Fixed [GLE Prediction] * Regression in version 2015 *: access violation on calculation with the models Henry Equation or Prausnitz/Shair if parameters are missing
- Fixed [VLE Prediction]: for several ternary (and higher) systems (e.g. Methanol + Water + Carbon dioxide) the prediction with PSRK and VTPR at constant pressure fails

Predictive EOS

- Fixed: some of the text output is mixing "." and "," as decimal separator if the default separator is not "."
- Fixed: the rubber-band in the plot is very slow

Process Synthesis

- Fixed [Entainer Selection] * Regression in version 2015 *: access violation in Absorption if "Gas Solubility Databank" is used as "Henry Coefficient Source"
- Fixed [ResidueCurves/AZEOT]: a switch from AZEOT to ResidueCurves and back clears AZEOT results

RecPar

• Fixed: access violation if datasets with 0 data points are added